



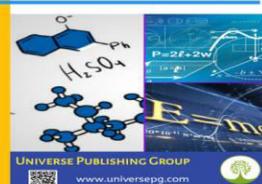
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## Magnetohydrodynamic Effects on the Flow of Nanofluids Across a Convectively Heated Inclined Plate Through a Porous Medium with a Convective Boundary Layer

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### ABSTRACT

The study explores the problem of Magnetohydrodynamic natural convection boundary layer flow of a nanofluid past a convectively heated inclined porous channel. The governing partial differential equations have been transformed through appropriate similarity functions into nonlinear ordinary differential equations. The emerging equations were solved numerically using both a sixth-order Runge-Kutta-Fehlberg and the shooting technique. The influences of pertinent parameters such as plate inclination angle, magnetic field, buoyancy ratio, and the convective heating term on the temperature, velocity, and concentration profiles were investigated graphically. Key findings indicate that an increase in magnetic field and permeability leads to a decline in the fluid's velocity while the temperature and nanoparticle concentration are significantly enhanced. The results obtained are in close correlation with existing body of knowledge discussed in the literature.

**Keywords:** MHD, Maple, Nonlinear, Nanofluid, Coupled ode, Nanoparticle, and Partial differential equations.

### INTRODUCTION:

The recent surge in nanofluid research has attracted scholar's interest worldwide, mostly due to its extensive applications in several industries, especially leading-edge businesses specialising in nano-devices. The utilisation of nanofluids has been extensively explored and documented in a substantial body of research, as referenced in (Goyal & Bhargara, 2014; Boungiorno, 2006; Al-Maman *et al.*, 2019; Muhamad *et al.*, 2023; Amer *et al.*, 2023; Ayub *et al.*, 2016). The rate of heat conduction and transfer in electronic equipment is very sluggish, which significantly hampers the operation of these systems. By incorporating nanoparticles such as copper (Cu) and alumina (Al) into a base fluid, the

efficiency of heat transfer can be improved, resulting in optimal performance of the device. For an extensive examination of the nanofluids in various shapes and conditions, refer to the scholarly publications cited in references (Al-Maman *et al.*, 2019; Muhamad *et al.*, 2023; Amer *et al.*, 2023; Goyal & Bhargara, 2014; Kuznetsov & Nield, 2018; Aziz *et al.*, 2012; Dhanal *et al.*, 2015; Ahmed & Elsaid, 2019; Alam *et al.*, 2015). These papers provide valuable perspectives on many subjects pertaining to nanofluid research and its practical implementations. The imperative to consistently pursue enhancement in thermal conductivity is unavoidable, considering that low thermal conductivity poses a significant barrier in the advancement of energy-efficient heat

transfer techniques, which are the vital in numerous applications.

Goyal and Bhargara, (2014) examined velocity slip boundary condition effect on the heat transfer flow of non-Newtonian nanofluids over a stretching sheet. According to the paper, there is a drop in heat and mass transfer rates as the slip parameter increases Dhanal *et al.* (2015). Conducted an investigation on the MHD boundary layer flow generated by the stretching and shrinking. According to the authors, viscous dissipation has a beneficial impact on heat and mass transmission, but Brownian motion has a minimal impact. The study conducted by Ali *et al.* (2021) demonstrated that as the concentration of Cu in water increases, the fluid velocity decreases, but the fluid temperature and concentration increases. This study examines the influence of a Cu-MHD hybrid nanofluid on heat transfer and flow in a permeable channel. The impacts of heat flux and viscous dissipation are taken into account, using a Newtonian base fluid. They observed that when the volume percentage grows, the velocity of the fluid increases while the temperature lowers. Additionally, the dissipation of viscosity contributes to an increase in the fluid's temperature. In a related development in Goyal and Bhargara, (2018) the boundary layer flow of a nanofluid was addressed using convective boundary conditions with magnetic effects. The Nusselt number was found to decrease when the inclination, buoyancy ratio, Brownian motion, and thermophoresis parameter rise, whereas it increases with an increased Prandtl number. References (Alam *et al.*, 2009; Ali *et al.*, 2013; Chen, 2004; Ali, 2012; Khan *et al.*, 2011) provide in-depth analysis of detail work on inclined planes, whereas references (Aziz & Khan, 2012; Aziz, 2009; Bejan, 2013; Narahari, 2013) address convective boundary problems.

The study conducted by Ghalambaz, (2014) investigated the spontaneous convection of nanofluids on a vertically oriented heated plate. It was noted that the thickness of the concentration profile is significantly smaller compared to the thickness of the temperature and velocity profiles. Additionally, it was observed that low convective heating leads to increased Brownian motion and affects the temperature profile. Conversely, Gunisetty *et al.* (2023) conducted research on the movement of nanofluid on a spinning disc, taking into account magnetic and radiative influences. Their primary

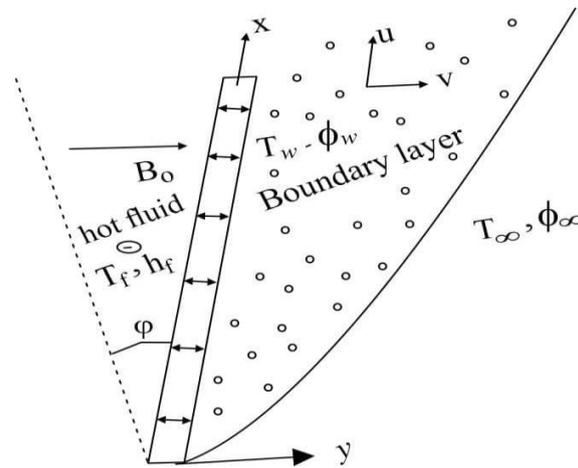
discoveries the demonstrated a positive correlation between the velocity profile and the Weissenberg number, and an increase in the electric field and radiative parameter resulted in an enhancement of the magnetic field and porosity. Detailed study on porosity is contained in (Ali *et al.*, 2012; Khan *et al.*, 2011; Mohebbi *et al.*, 2020; Olanrewaju *et al.*, 2013). This study draws inspiration from the array of literature discussed above. Many researchers have extensively studied many facets of nanofluids due to its wide-ranging utilisation in the contemporary technological era, where efficient heat transmission has significant impact (Akter *et al.*, 2023).

Nevertheless, despite the numerous factors taken into account by multiple authors, there has been limited focus on the study of natural convection nanofluid flow over an inclined porous plate subjected to the convective heating and influenced by a magnetic field. Essentially, this article delves into this novel concept. The mathematical modeling incorporated factors such as the uniform magnetic field, the permeability, and convective boundary conditions, among other considerations. The equations that describe the flow dynamics are derived and then converted into non-dimensional forms using suitable similarity functions. The numerical computations are performed by utilising MAPLE solver. Findings are depicted through graphs and tables, analysed and discussed intuitively

### Mathematical Formulation

A two-dimensional, laminar, stable, and incompressible flow with constant physical properties is considered. The semi-infinite plate is subjected to inclination  $\varphi$  along the vertical axis. The flow direction is tailored towards the horizontal axis, with a constant magnetic field  $B_0$  in the vertical direction. It is assumed that the lower part of the plate is thermally heated by convection through a hot fluid at a temperature  $T_f$  with a heat transfer coefficient  $h_f$ . Further, the base fluid and nanoparticles are considered to be in thermal equilibrium. The schematic depiction of the formulation is thus demonstrated.

The continuity, momentum, energy, and nanoparticle concentration equations in Goyal and Bhargara, (2018) below serve as the governing equations for the flow under the aforementioned presumptions.



**Fig. 1:** Model configuration.

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \tag{1}$$

$$\rho f \left( u \frac{\partial u}{\partial x} + v \frac{\partial v}{\partial y} \right) = \mu \frac{\partial^2 u}{\partial y^2} - \sigma_n B_0^2 u - \frac{\mu}{\rho k} u + [(1 - \phi_\infty) \rho f_\infty \beta g_e (T - T_\infty) - (\rho_p - \rho f_\infty) g_e (\phi - \phi_\infty)] \cos \phi \tag{2}$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha_m \frac{\partial^2 T}{\partial y^2} + \tau \left[ D_B \frac{\partial \phi}{\partial y} \frac{\partial T}{\partial y} + \frac{D_T}{T_\infty} \left( \frac{\partial T}{\partial y} \right)^2 \right] \tag{3}$$

$$u \frac{\partial \phi}{\partial x} + v \frac{\partial \phi}{\partial y} = D_B \frac{\partial^2 \phi}{\partial y^2} + \frac{D_T}{T_\infty} \frac{\partial^2 T}{\partial y^2} \tag{4}$$

Where  $u$  and  $v$  are the velocity components perpendicular to the plate and parallel to it, respectively;  $B_0$  is the magnetic field;  $\phi$  is the volume fraction of the nanoparticles;  $\beta$  is the thermal expansion coefficient of the base fluid;  $\phi$  is the angle of inclination;  $D_B$  is

the Brownian diffusion coefficient;  $D_T$  is the thermophoretic diffusion coefficient; and  $T$  is the dimensional temperature. The boundary conditions we propose are;

$$u = 0, v = 0, \phi = \phi_w, -k \frac{\partial T}{\partial y} = h_f (T_f - T) \text{ at } y = 0 \tag{5}$$

$$u = 0, v = 0, \phi = \phi_\infty, T = T_\infty \text{ as } y \rightarrow \infty \tag{6}$$

With  $u = \partial \psi / \partial y$  and  $v = -\partial \psi / \partial x$ , equation (1) is identically satisfied. We deployed the similarity variables below to Equations (2)- (6);

$$\eta = \frac{y}{x} Ra_x^{\frac{1}{4}}, \psi = \alpha_m Ra_x^{\frac{1}{4}} f(\eta), \theta(\eta) = \frac{T - T_\infty}{T_f - T_\infty}, \phi(\eta) = \frac{\phi - \phi_\infty}{\phi_f - \phi_\infty} \tag{7}$$

Where the local Rayleigh number is expressed as

$$Ra_x = \frac{(1 - \phi_\infty) \beta g_e (T_f - T_\infty) x^3}{\nu \alpha_m} \tag{8}$$

Using Eqs. (7), and (8) in Eqs. (2)- (6), we have the equations;

$$f''' + \frac{1}{4Pr} (3ff'' - 2f'^2) + (\theta - Nr\phi) \cos \phi - (M + K)f' = 0 \tag{9}$$

$$\theta'' + \frac{3}{4}f\theta' + N_b\theta'\phi' + N_t\theta'^2 = 0 \tag{10}$$

$$\phi'' + \frac{N_t}{N_b}\theta'' + \frac{3}{4}Lef\phi' = 0 \tag{11}$$

The associated boundary conditions are transformed to the following;

$$f(\eta) = 1, f'(\eta) = 0, \theta'(\eta) = -NC[1 - \theta(\eta)], \phi(\eta) = 1 \text{ at } \eta = 0 \tag{12}$$

$$f'(\eta) = 0, \theta(\eta) = 0, \phi(\eta) = 0 \text{ as } \eta \rightarrow \infty \tag{13}$$

In the context of equations (9) - (13), prime represent differentiation with respect to  $\eta$ ,  $P_r$  Prandtl number,  $N_r$  Buoyancy-ratio parameter,  $L_e$  nanoparticle Lewis number  $N_c$  convective heating parameter,  $K$  the

permeability parameter and  $M$  magnetic parameter. The parameters are the mathematically represented below Goyal and Bhargara, (2018).

$$P_r = \frac{\mu}{\alpha_m}, N_r = \frac{(\rho_p - \rho_f)(\phi_w - \phi_\infty)}{\rho_f(1 - \phi_w)(T_f - T_\infty)}, M = \frac{\sigma B_0^2 x^3}{\mu R a_x^2}, N_c = \frac{h x^{\frac{1}{4}}}{k} \left[ \frac{v \alpha_m}{(1 - \phi_\infty) g_e \beta (T - T_\infty)} \right]^{\frac{1}{4}}, K = \frac{v}{a k} \tag{14}$$

It is crucial to remark that the assessment of nano-fluidic device performance necessitates a thorough consideration of heat and mass transmission. Hence, it is imperative to consider two essential physical parameters pertaining to the rates of heat and mass

transport, as indicated by Siddiqua *et al.* (2014). The Local Nusselt number, denoted as  $Nux$ , and the Sherwood number, denoted as  $Shx$ , is mathematically represented as follows.

$$Nu_x = \frac{x q_w}{k(T_f - T_\infty)}, Sh_x = \frac{x j_w}{D_B(\phi_w - \phi_\infty)} \tag{15}$$

In the context of equation (15);

$q_w$  = heat flux from the plate

$j_w$  = mass flux from the plate

These terms are mathematically defined as;

$$q_w = -k \left( \frac{\partial T}{\partial y} \right), j_w = -D_B \left( \frac{\partial C}{\partial y} \right) \text{ at } y = 0 \tag{16}$$

With equations (7) and (8), the dimensionless parameters take the form expressed in equation (17)

$$Ra_x^{\frac{1}{4}} Nu_x = -\theta'(0), Ra_x^{\frac{1}{4}} Sh_x = -\phi'(0) \tag{17}$$

**Method of Solution**

Equations (9-11), subject to Eqs. (12), and (13) were numerically treated with Maple Solver. The default numerical solution methods employed by the software for two-point boundary value problems involve the utilisation of a sixth-order Runge-Kutta Fehlberg method in conjunction with shooting techniques. The effectiveness of these strategies has been substantiated by scholarly publications Olanrewaju *et al.* (2013). A comprehensive examination of our findings is presented in the next section.

**RESULTS AND DISCUSSION:**

In this section, we provide graphical figures and a comprehensive discussion to the enhance the under-

standing of the physical aspects of this work. The obtained results are graphically shown in terms of velocity, temperature, and concentration profiles. Tables showing the computations of local Nusselt and Sherwood numbers and a diverse set of relevant parameters are shown. As seen in **Table 1**, the computed value decreases the monotonically for different values of the Prandlt number. This shows a clear correlation with the results articulated in (Bejan, 2013; Kuznetsov and Nield, 2010). In **Table 2**, the computation of  $Nux$  and  $Shx$  numbers under the influence of several pertinent parameters is presented. Results are in close correlation compare to Aziz and Khan, (2012). The dependency of the Nuselt and Sherwood numbers over variations in  $P_r$ ,

$Nb$ , and  $Nr$  with other parameters fixed is presented. It is seen that Nusselt and Sherwood numbers increases as  $Pr$  increases whereas for fixed  $Pr$ , both decreases monotonically as  $Nb$  and  $Nr$  increases. The changes in the Magnetic field parameter, thermophoresis parameter, and the Plate's inclination angle on  $Nux$  and  $Shx$  numbers is depicted in **Table 4**. The performance of heat and transfer decreases as the plate's inclination angle and the magnetic field are steadily increased. The corresponding value of  $Nt$  are equally represented in **Table 4**. **Fig. 2, 3, and 4** depict the impact of the magnetic field  $M$  on the dimensionless velocity, temperature, & concentration, correspondingly. The data presented indicates a decrease in the velocity profile for increased magnetic field strength, while temperature and concentration are both enhanced. This implies that the Lorentz force, which is a type of resistive force, was generated due to the presence of a magnetic field. The force appears to impede the accumulation of momentum thereby decelerating the fluid flow and opposing the influence of  $M$ . The thermal energy is generated as a result of the increased force used during the process of pulling the nanofluid. The energy transfer leads to an increase in the temperature of the nanofluid. As a result, the presence of the magnetic field causes a reduction in the thickness of the momentum boundary layer and an augmentation in the thickness of the thermal boundary layer.

Furthermore, the phenomenon of the nanoparticle diffusion is facilitated by the warming of the boundary layer, resulting in an elevation of the concentration of the fluid, as depicted in **Fig. 4**. **Fig. 5, 6, and 7** depict the effect of the porosity parameter on the fluid's dimensionless velocity, temperature, and concentration profiles. Clearly, it is observed that the velocity diminishes as porosity increases. In practice, this means that higher values of porosity are indicative of increased viscous forces, which lead to a dominance of initial forces, which in turn causes the velocity to decrease. However, a gradual increase in porosity value leads to an observable enhancement in both the dimensionless temperature and concentration (see **Fig. 6 and 7**). Furthermore, the decrease in fluid velocity occasioned by an increase in porosity can be explained more by the presence of porous medium. This medium introduces obstructions and resistance to the flow of the fluid. The medium gradually gets more obstructive as the porosity parameter rises, resulting in increased resistance, Universe PG | [www.universepg.com](http://www.universepg.com)

which finally causes a decrease in the fluid's velocity. In **Fig. 8**, the influence of nanofluid Lewis number on the dimensionless concentration is presented and shows a sharp decline in concentration of the nanoparticles as  $Le$  increase. Practically, for a base fluid of certain thermal diffusivity  $D_B$ , a higher  $Le$  indicates a lower Brownian diffusion coefficient, resulting in a shorter penetration depth for the concentration boundary layer. The word "thermophoresis" describes how particles disperse when there is a temperature gradient present. **Fig. 9 and 10** show, respectively, how the thermophoresis parameter  $Nt$  affects the dimensionless temperature and concentration. It goes without saying that altering  $Nt$ 's value causes a rise in the temperature gradient and a strengthening of the force within nanoparticles. This force causes more fluid to the heat up, which likewise boosts the temperature. Enhancing the thermophoresis  $Nt$  effect yields a similar outcome for nanoparticle concentration, as shown in **Fig.10**. Due to constant collisions between nanoparticles and base fluid molecules, Brownian motion is the zigzag movement of nanoparticles inside the base fluid. **Fig. 11 and 12** demonstrate the effect of  $Nt$  on temperature and concentration. The randomness of the nanoparticles is seen to increase rapidly in a chaotic manner as  $Nb$  increases. This chaotic behaviour causes more collisions in the system. This increased collision of nanoparticles causes an increase in heat transfer properties and thus increases the temperature of the fluid. Similarly, the concentration of nanoparticles along the wall is hampered by a concurrent increase in  $Nb$ . As a result, the value of the nanoparticle concentration along the wall decreases as the nanoparticles shift from the boundary to the fluid by increasing their random motion. The impact of the convective heating parameter  $Nc$  on the velocity is examined in **Fig. 13**. A rise in  $Nc$  increases the fluid's velocity, as shown in the figure. The effects of plate inclination angle from vertical for values of  $0^0, \frac{\pi}{10}, \frac{\pi}{9},$  and  $\frac{\pi}{6}$  on the dimensionless velocity, temperature, and concentration are shown in **Fig. 14, 15, and 16**, respectively. The fluid's velocity decreases along with the boundary layer as the plate inclination angle  $\varphi$  is changed. The alignment of the plate is what creates the effect, through the buoyancy term in equation 2. The value of  $\text{Cos } \varphi$  falls in proportion as the value of  $\varphi$  grows. This results in the buoyancy effect disappearing as the plate's inclination angle  $\varphi$  increases. As a result, the driving force acting on the

fluid weakens, lowering its velocity. This observation corresponds well with Alam *et al.* (2009) in terms of velocity profile. Also, **Fig. 15** and **16** clearly reflect how the depletion of the buoyancy effect enhances thermal and nanoparticle diffusion with a variation in the plate's inclination  $\phi$ . **Fig. 17**,

**18**, and **19** show the characteristics behaviour of the buoyancy ratio parameter on the dimensionless velocity, temperature, & concentration. As observed in the figures, while increase in the buoyancy parameter enhances the fluid's temperature and concentration, it depletes the velocity.

**Table 1:** Comparison of  $Nu_x$  of regular fluid for various values of  $Pr$  with  $Le = 10, Nb = Nt = 10^{-5}, NC = 10, \phi = k = 0$ .

$Pr$	Bejan, (2013)	Kuznetsov & Nield, (2010)	Narahari, (2013)	Present Result
1	0.401	0.401	0.401	0.566
10	0.465	0.463	0.459	0.665
100	0.490	0.481	0.473	0.694
1000	0.499	0.484	0.474	0.699

**Table 2:** Comparison of results for  $Nu_x$  and  $Sh_x$  for  $Nt = 0.1, NC = Le = 10, m = k = \phi = 0$ .

$Nb$	$Nr$	$Pr = 1.0$				$Pr = 5.0$			
		$Nu_x$		$Sh_x$		$Nu_x$		$Sh_x$	
		Aziz & Khan, (2012)	Present results						
0.1	0.1	0.3396	0.4578	0.9954	2.0413	0.3807	0.4792	1.0608	2.1747
	0.2	0.3366	0.4571	0.9828	2.0380	0.773	0.4788	1.0482	2.1713
	0.3	0.3334	0.4564	0.9697	2.0346	0.3739	0.4785	1.0351	2.1679
	0.4	0.3301	0.4557	0.9559	2.0312	0.3702	0.4781	1.0214	2.1643
	0.5	0.3267	0.4540	0.9414	2.0271	0.3665	0.4778	1.0071	2.1608
0.3	0.1	0.2939	0.388	1.0435	2.1204	0.3306	0.4069	1.1101	2.2368
	0.2	0.2918	0.3875	1.0317	2.1176	0.3282	0.4066	1.0985	2.2339
	0.3	0.2896	0.3871	1.0195	2.1147	0.3258	0.4063	1.0866	2.2310
	0.4	0.2872	0.3867	1.0067	2.1110	0.3232	0.4061	1.0741	2.2282
	0.5	0.2848	0.3862	0.9934	2.1091	0.3206	0.4058	1.0611	2.2253
0.5	0.1	0.2530	0.3271	1.0584	2.1366	0.2855	0.3437	1.1263	2.2496
	0.2	0.2513	0.3267	1.0471	2.1334	0.2836	0.3435	1.1152	2.2469
	0.3	0.2495	0.3264	1.0353	2.1311	0.2816	0.3432	1.1037	2.2442
	0.4	0.2477	0.3261	1.0230	2.1284	0.2796	0.3431	1.0918	2.2415
	0.5	0.2458	0.3257	1.0102	2.1257	0.2775	0.3429	1.0794	2.2387

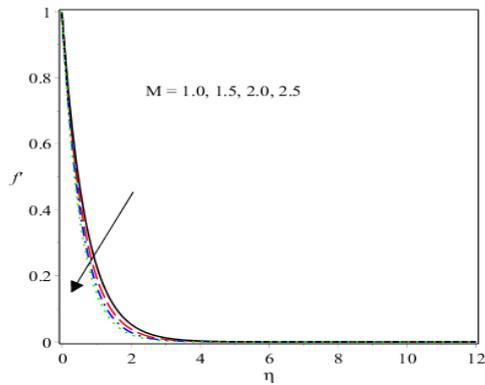
**Table 3:** Variations of  $Nu_x$  and  $Sh_x$  for  $M, Nt$  and  $\phi$  when  $Nc = 10, Pr = 5.0, Nb = Nr = 0.5, Le = 10, K = 1.0$ .

$Nt$	$\phi$	$m = 1.0$		$m = 1.2$		$m = 1.5$	
		$Nu_x$	$Sh_x$	$Nu_x$	$Sh_x$	$Nu_x$	$Sh_x$
0.1	0	0.2127	1.9490	0.2095	1.9332	0.2049	1.9093
	$\frac{\pi}{10}$	0.2054	1.9232	0.2021	1.9077	0.1973	1.8856
	$\frac{\pi}{9}$	0.1986	1.9022	0.1951	1.8868	0.1902	1.8649
	$\frac{\pi}{6}$	0.1897	1.8786	0.1860	1.8634	0.1809	1.8417
0.3	0	0.1623	1.9783	0.1614	1.9602	0.1591	1.9349
	$\frac{\pi}{10}$	0.1586	1.9456	0.1570	1.9280	0.1545	1.9034
	$\frac{\pi}{9}$	0.1541	1.9192	0.1523	1.9020	0.1493	1.8779
	$\frac{\pi}{6}$	0.1477	1.8898	0.1453	1.8730	0.1419	1.8944
0.45	0	0.1226	2.0248	0.1233	2.0041	0.1236	1.9753
	$\frac{\pi}{10}$	0.1226	1.9846	0.1224	1.9648	0.1217	1.9373

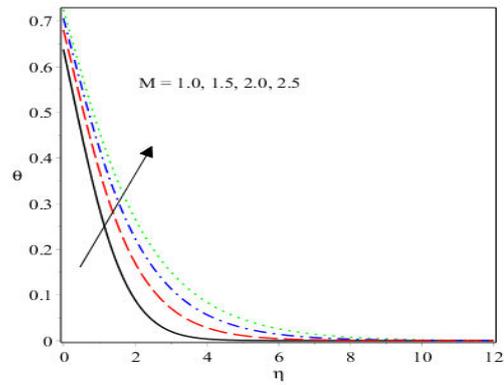
	$\frac{\pi}{9}$	0.1206	1.9526	0.1198	1.9335	0.1184	1.9069
	$\frac{\pi}{6}$	0.1161	1.9173	0.1147	1,8989	0.1126	1.8731

**Table 4:** Variations of  $Nu_x$  and  $Sh_x$  for  $Pr, Nb$  and  $Nr$  when  $Nt = 0.1, \varphi = \frac{\pi}{6}, Le = 10, K = 1.0, NC = K = M = 1.0, Le = 10, K = 1.0$ .

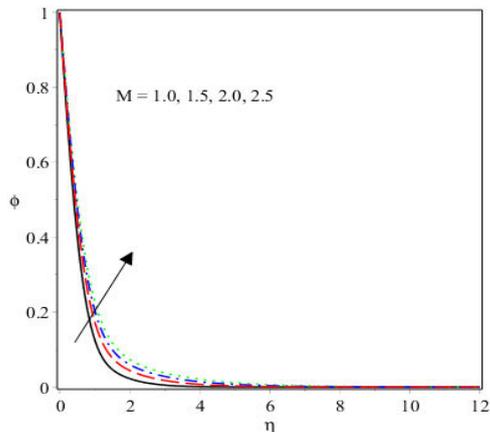
$Nb$	$Nr$	$Pr = 1.0$		$Pr = 5.0$		$Pr = 10.0$	
		$Nu_x$	$Sh_x$	$Nu_x$	$Sh_x$	$Nu_x$	$Sh_x$
0.1	0.1	0.2417	1.7657	0.2520	1.8037	0.2534	1.8088
	0.2	0.2415	1.7649	0.2518	1.8029	0.2532	1.8080
	0.3	0.2414	1.7641	0.2516	1.8021	0.2530	1.8072
	0.4	0.2412	1.7634	0.2514	1.8013	0.2528	1.8064
	0.5	0.2410	1.7626	0.2512	1.8005	0.2526	1.8056
	0.6	0.2408	1.7618	0.2511	1.7998	0.2525	1.8048
0.3	0.1	0.2104	1.8319	0.2198	1.8682	0.2211	1.8730
	0.2	0.2102	1.8312	0.2197	1.8675	0.2210	1.8723
	0.3	0.2101	1.8305	0.2196	1.8668	0.2209	1.8716
	0.4	0.21006	1.8299	0.2195	1.8662	0.2208	1.8710
	0.5	0.2099	1.8292	0.2193	1.8655	0.2201	1.8703
	0.6	0.2098	1.8285	0.2192	1.8648	0.2206	1.8696
0.5	0.1	0.1815	1.8453	0.1901	1.8813	0.1918	1.8860
	0.2	0.1814	1.8446	0.1900	1.8806	0.1913	1.8854
	0.3	0.1813	1.8440	0.1899	1.8799	0.1918	1.8847
	0.4	0.1812	1.8433	0.1898	1.8793	0.1910	1.8841
	0.5	0.1811	1.8427	0.1897	1.8786	0.1909	1.8834
	0.6	0.1811	1.8420	0.1896	1.8780	0.1908	1.8822



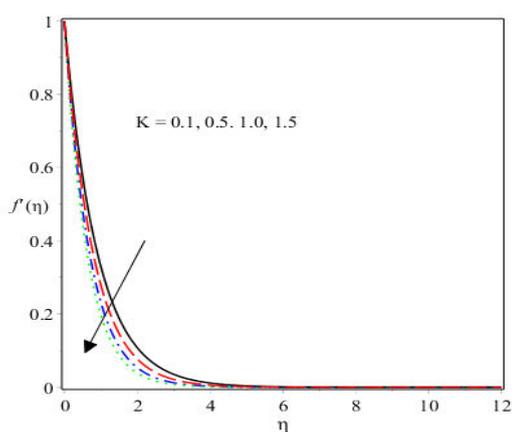
**Fig. 2:** Effect of  $M$  on velocity.



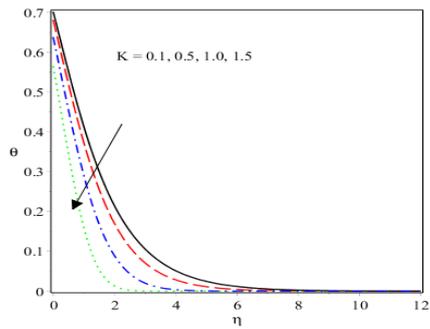
**Fig. 3:** Effect of  $M$  on temperature.



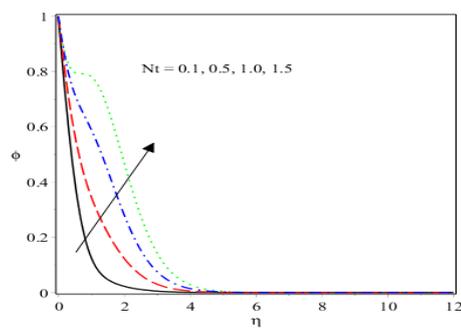
**Fig. 4:** Effect of  $M$  on concentration.



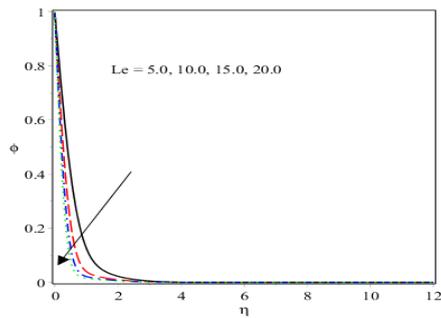
**Fig. 5:** Effect of  $K$  on velocity.



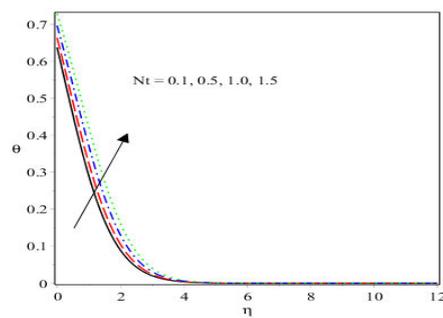
**Fig. 6:** Effect of  $K$  on temperature.



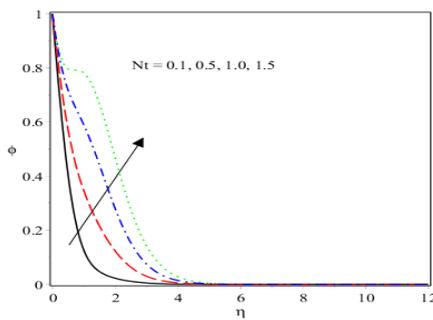
**Fig. 7:** Effect of  $K$  on concentration.



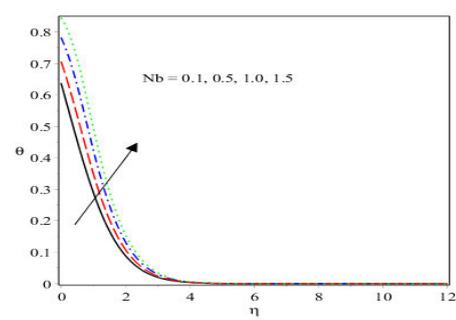
**Fig. 8:** Effect of  $Le$  on concentration.



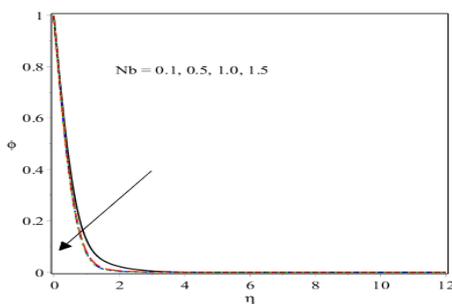
**Fig. 9:** Effect of  $Nt$  on temperature.



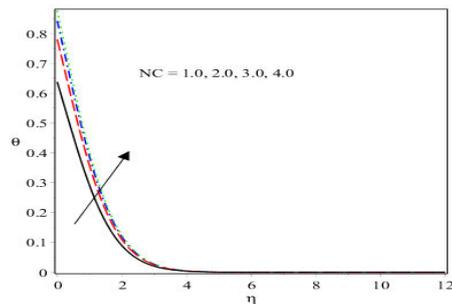
**Fig. 10:** Effect of  $Nt$  on concentration.



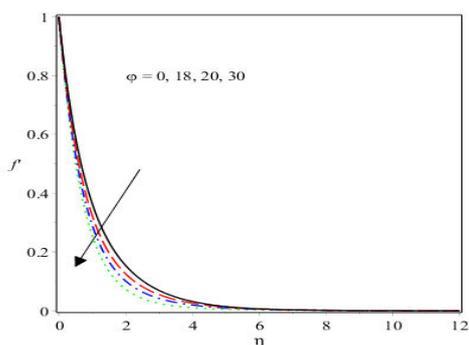
**Fig. 11:** Effect of  $Nb$  on temperature.



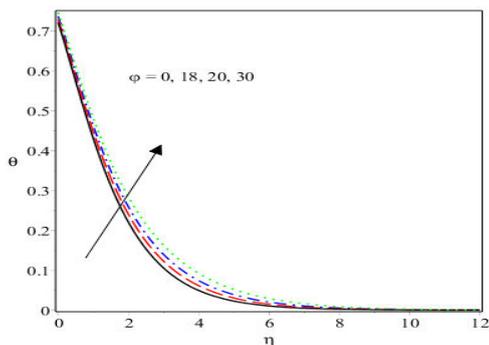
**Fig. 12:** Effect of  $Nb$  on concentration.



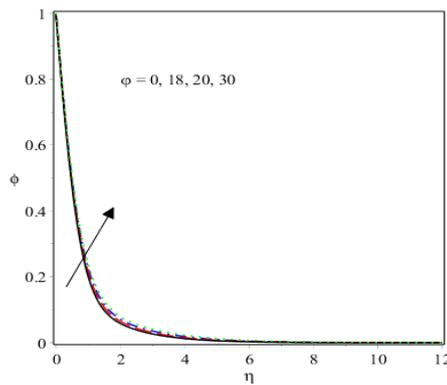
**Fig. 13:** Effect of  $NC$  on temperature.



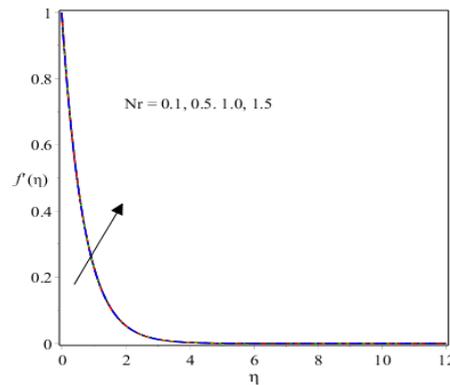
**Fig. 14:** Effect of plate inclination  $\phi$  on velocity.



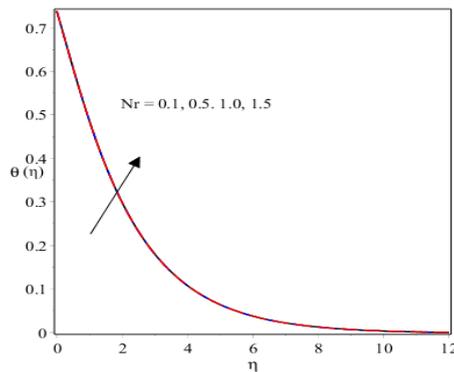
**Fig. 15:** Effect of plate inclination  $\phi$  on temperature.



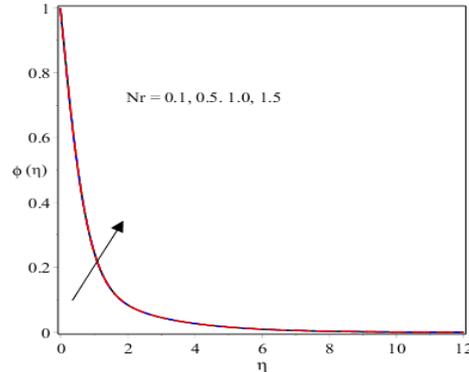
**Fig. 16:** Effect of  $\phi$  on concentration.



**Fig. 17:** Effect of  $Nr$  on velocity.



**Fig. 18:** Effect of  $Nr$  on Temperature.



**Fig. 19:** Effect of  $Nr$  on concentration.

**CONCLUSION:**

The following conclusions are interesting drawn from this article. The inclusion of the convective boundary condition, as opposed to the usual continuous heat flux, is a novel idea (see Fig. 13). This phenomenon is relevant in heat exchanger systems where fluid flow through a solid surface affects the solid surface's conduction. As the permeability of the plate rises, a decrease in nano-fluid temperature is seen. Convective heating, Brownian motion, and thermophoresis parameters, on the other hand, show the opposite pattern. As magnetic field, permeability, and plate inclination values rise, the nanofluid velocity profile decreases. An increase in the Brownian motion parameter decreases the nanoparticle concentration, but contrasting observations are noticed in the case of the thermophoresis parameter. As the plate inclination increases, nanoparticle temperature and concentration are enhanced, in contrast to the nano-particle velocity. That is the momentum the boundary layer decays. As the magnetic field increases, the thermal and the nanovolume fraction boundary layers grow while the momentum the boundary layer thickness decreases. The Lorentz force, which is created by the magnetic field, slows down fluid motion. Therefore, the heat transmission can be evaluated by the appropriately adjusting M. Universe PG | [www.universepg.com](http://www.universepg.com)

Cooling devices frequently use this idea. By taking into account various base fluid and nanoparticle combinations, heat and mass transfer rates can be lowered. This idea applies by modifying the heat transfer rates for industries that use inclined plates during production. However, this study focused on steady state nano-fluid flow and the associated parameters of interest. Subsequent studies will expand on this study by examining a time dependent flow of nanofluid over an inclined heated plate with the inclusion of the joule-heating and other considerations.

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**CONFLICTS OF INTEREST:**

The authors declare no conflict of interest.

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